

Heat Recovery at Alaska Center for Energy and Power



ACEP
Alaska Center for Energy and Power

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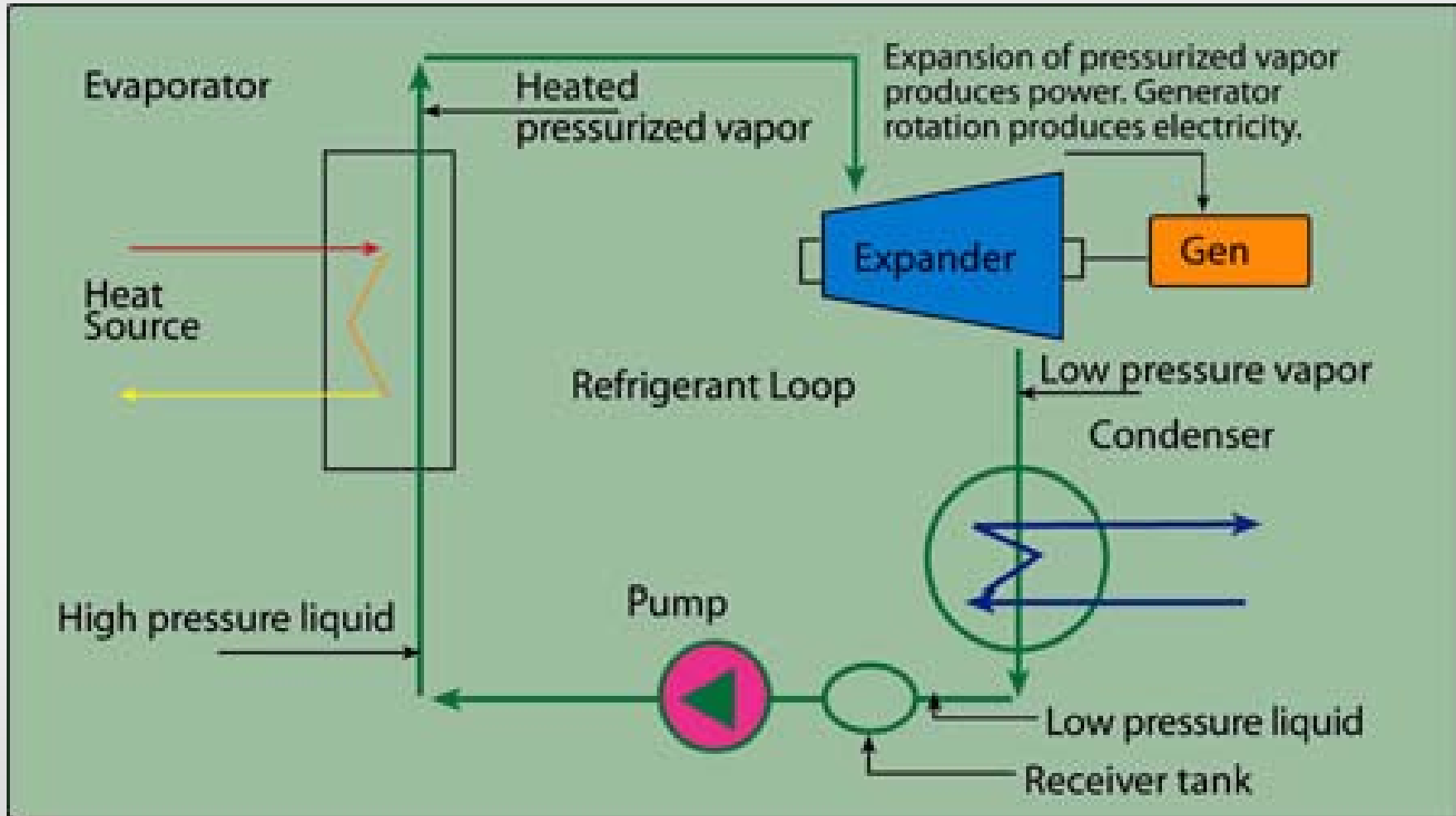
University of Alaska Fairbanks

Organic Rankine Cycle

- Power generation through use of an Organic Rankine Cycle (ORC) unit with heat recovery from diesel generator.
- Laboratory and field tests.
- Funded by Denali Commission and Alaska Energy Authority.



ORC Technology



Project objectives:

- To achieve ORC efficiency of 10% and corresponding fuel efficiency by ~3%.
 - Reduced fuel consumption
 - Lower costs
 - Reduced greenhouse gas emissions
- To evaluate feasibility, operation / maintenance requirements, and economic impact.
- To develop guidelines for ORC application, particularly in rural Alaska.

Effect of ORC on overall efficiency

Starting engine fuel efficiency (kw-hr/gal)	14.5	14.5	14.5
Gal fuel per 1000 kW-hr	68.9655	68.9655	68.9655
Cost per 1000 kW-hr (at \$6.50/gal)	\$448.28	\$448.28	\$448.28

ORC efficiency improvement (%)	10	9	5
ORC fuel efficiency improvement (kW-hr/gal)	1.6675	1.50075	0.83375
Net fuel efficiency (kW-hr/gal)	16.1675	16.00075	15.33375
Gal fuel per 1000 kW-hr	61.8525	62.4971	65.2156
Cost per 1000 kW-hr (at \$6.50/gal)	\$402.04	\$406.23	\$423.90

Cost savings	\$46.24	\$42.05	\$24.38
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Potential cost savings

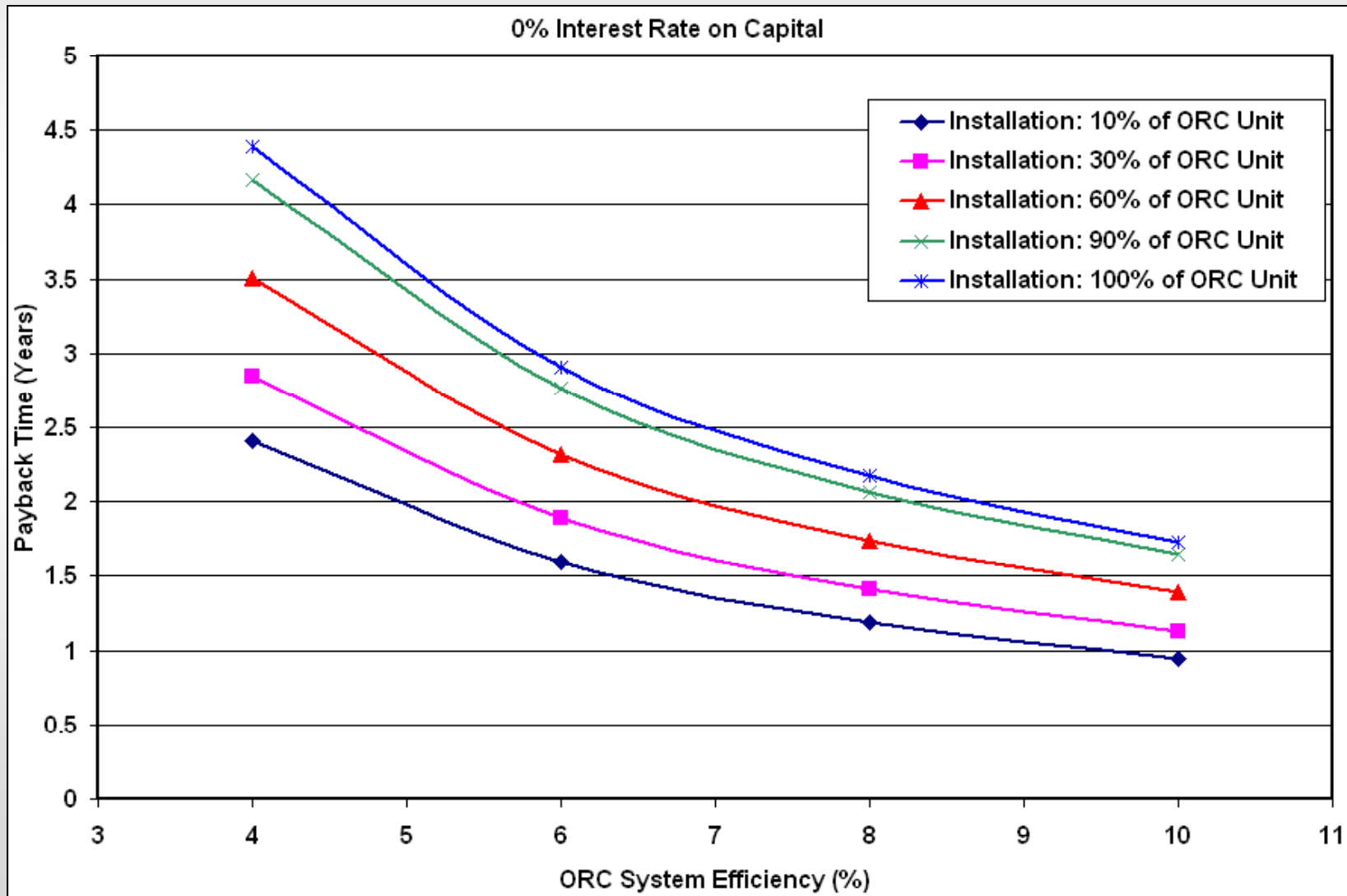
ORC efficiency improvement (%)	10	9	5
Cost savings per 1000 kW-hr/gal	\$46.24	\$42.05	\$24.38

Hypothetical community with power generation = 4 million kW-hr

Potential annual savings with ORC	\$184,960	\$168,200	\$97,520
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Economic Analysis (payback time)

ORC unit cost = \$128,000 / Fuel efficiency = 14 kw-hr/gal



ORC qualifies as “emerging technology” ...

- ORC technology currently used in large-scale and industrial applications around the world.
- Few data exist on small-scale applications.
- NO data in Alaska.
- Alaska has unique environmental and climatic conditions. Rural villages have unique operating conditions.
- There is a need for laboratory / field performance data for optimal application and design improvement.

Heat Recovery Study

Heat Recovery from Diesel Exhaust for Heating

1. Experimental study of feasibility, performance, and economic analysis.
2. Development of a design and economic analysis computer program for rural power plant engineers to conduct preliminary design and determine whether applying exhaust heat for heating to any of the village power plants is beneficial.
(Complete)

Heat Recovery for Power

1. Experimental study of feasibility, performance, and economic analysis.
2. Development of a tool to make comments on design, to help laying out test plan.
3. Development of system maps for selecting appropriate diesel generator and optimizing the system performance (for different engine operating and environmental conditions).

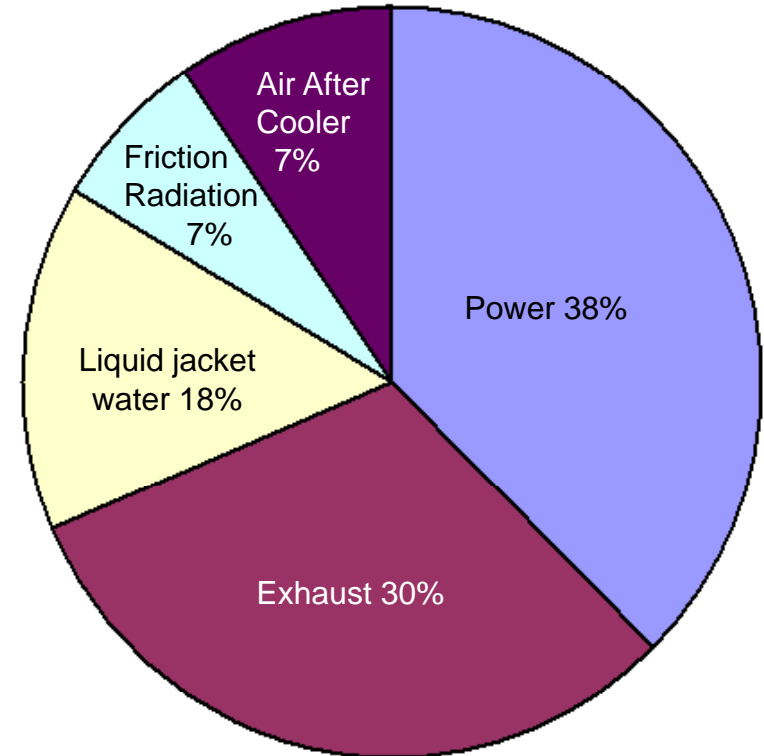
Potential

Exhaust Heat energy recovery for heating:

- Heat recovery: 15% fuel energy
- Fuel savings: 15% fuel used by engine
- Winter season only
- Restricted application (Only for heating)

Heat energy recovery for power (for generator set average load less than about 1 MW):

- Engine efficiency improvement: About 4%
- Fuel savings: About 10% (14.5kW-hr/gallon)
- May be for the whole year
- Flexibility in application

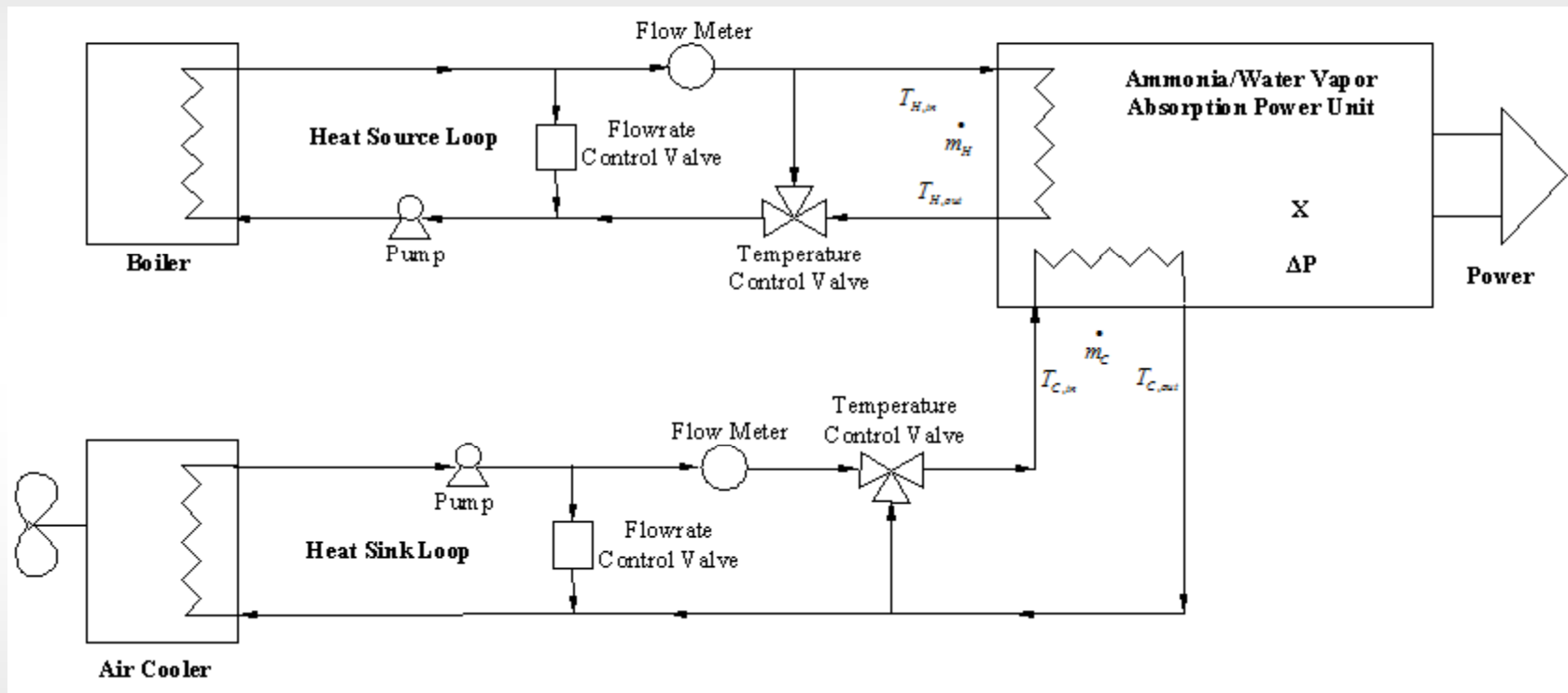


Other Considerations

- **Infrastructure in existing power and heating systems.**
- **Load patterns in power and heating usages.**
- **Environmental and surrounding conditions (i.e. temperatures, stream, etc.).**
- **Operation loss.**
- **Performance characteristics of individual technologies (e.g. working fluid, positive pressure cooling).**

Research is needed for the development of appropriate methods and tools to assist the selection of best fit technology to optimize the benefit to individual villages.

Heat Recovery Unit for Power: General Components in Application



Heat Recovery for Power

Ammonia –water system (VS ORC):

Theoretically it is more efficient (Need real life data to approve it).

It can use positive pressure for cooling side.

It needs a separator and an absorber.

Other factors needs to be considered include:

- Heat exchanger design.

- Ammonia concentration limit (at high ambient temperature).

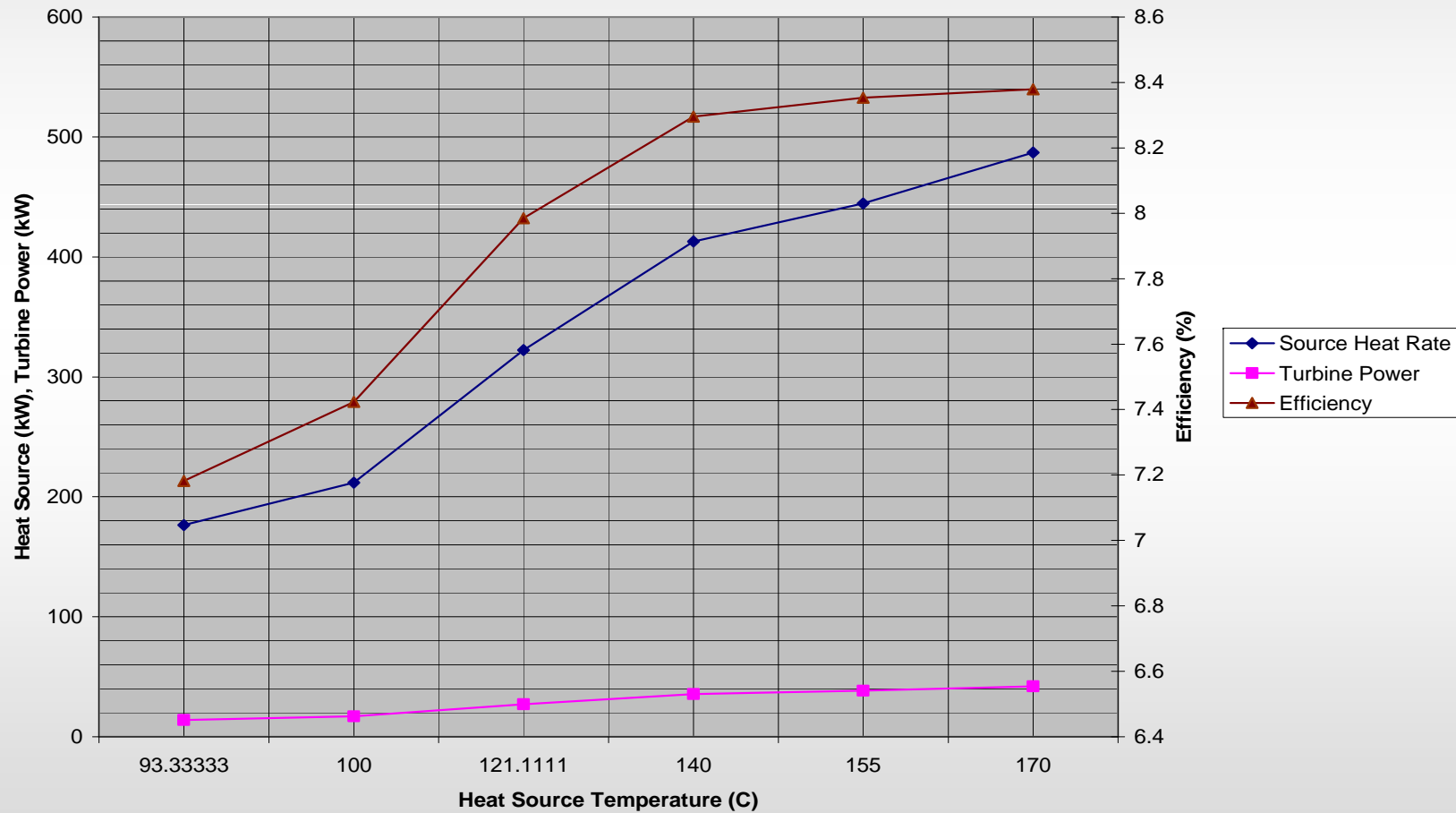
- Etc.

Current Projects: Ammonia-Water Cycle



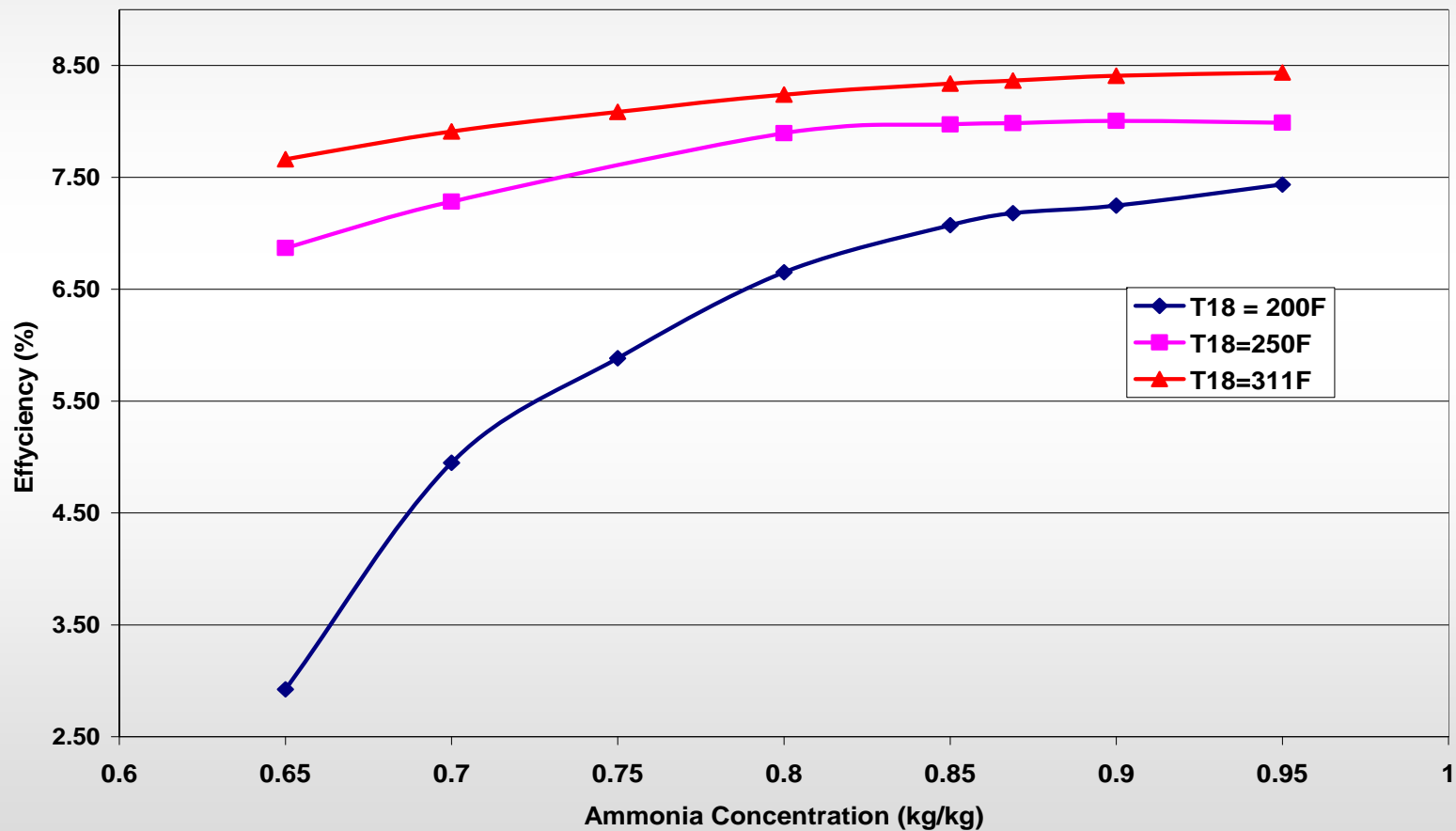
Heat Source: System Performance VS Heat Source Temperatures with Ammonia Concentration X= 0.87

Performance at Different Heat Source Temperatures (X= 0.87)

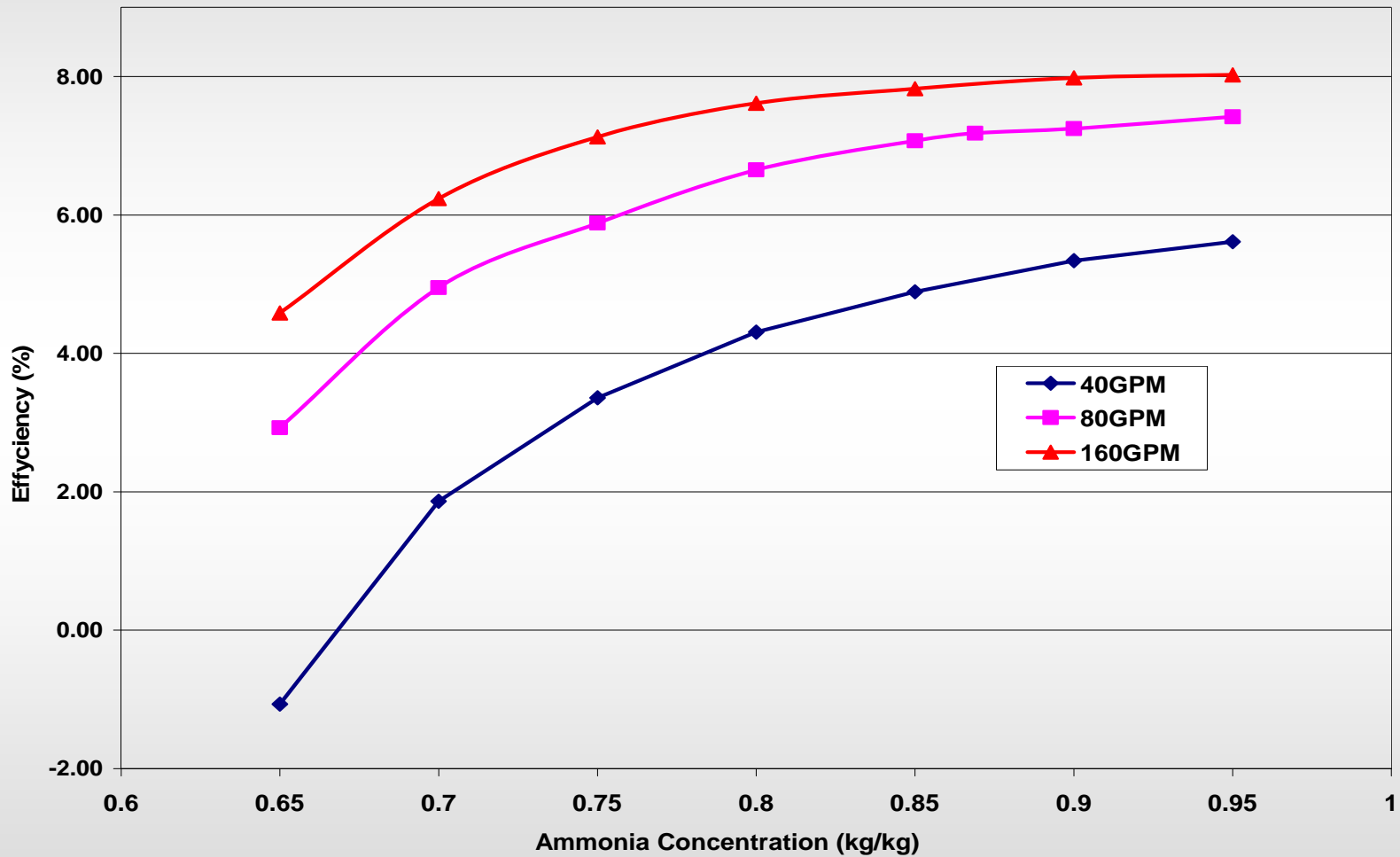


Heat Source: Efficiency versus Ammonia Concentration and Source Temperatures

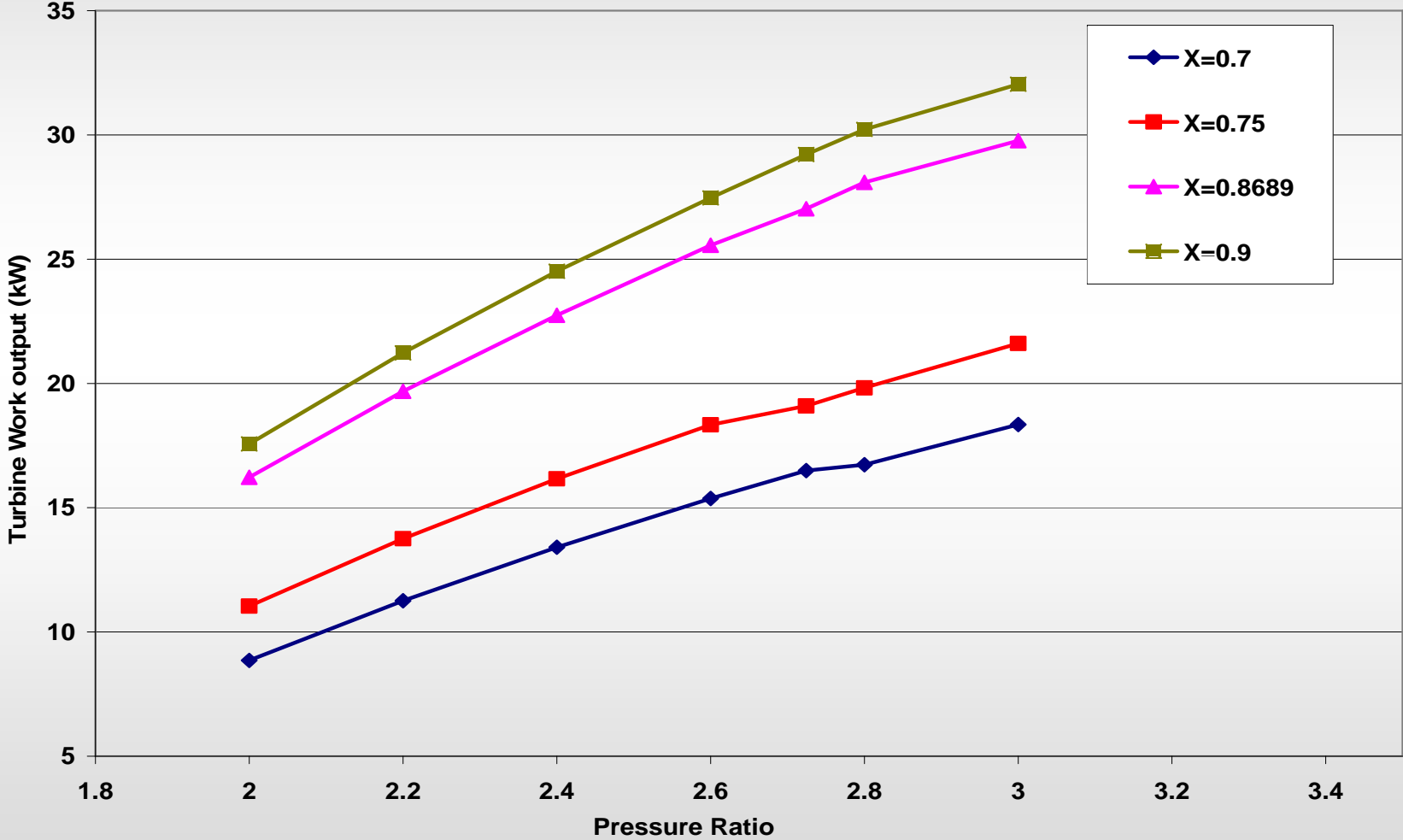
Efficiency versus Ammonia Concentration for Different Heat Source Temperatures



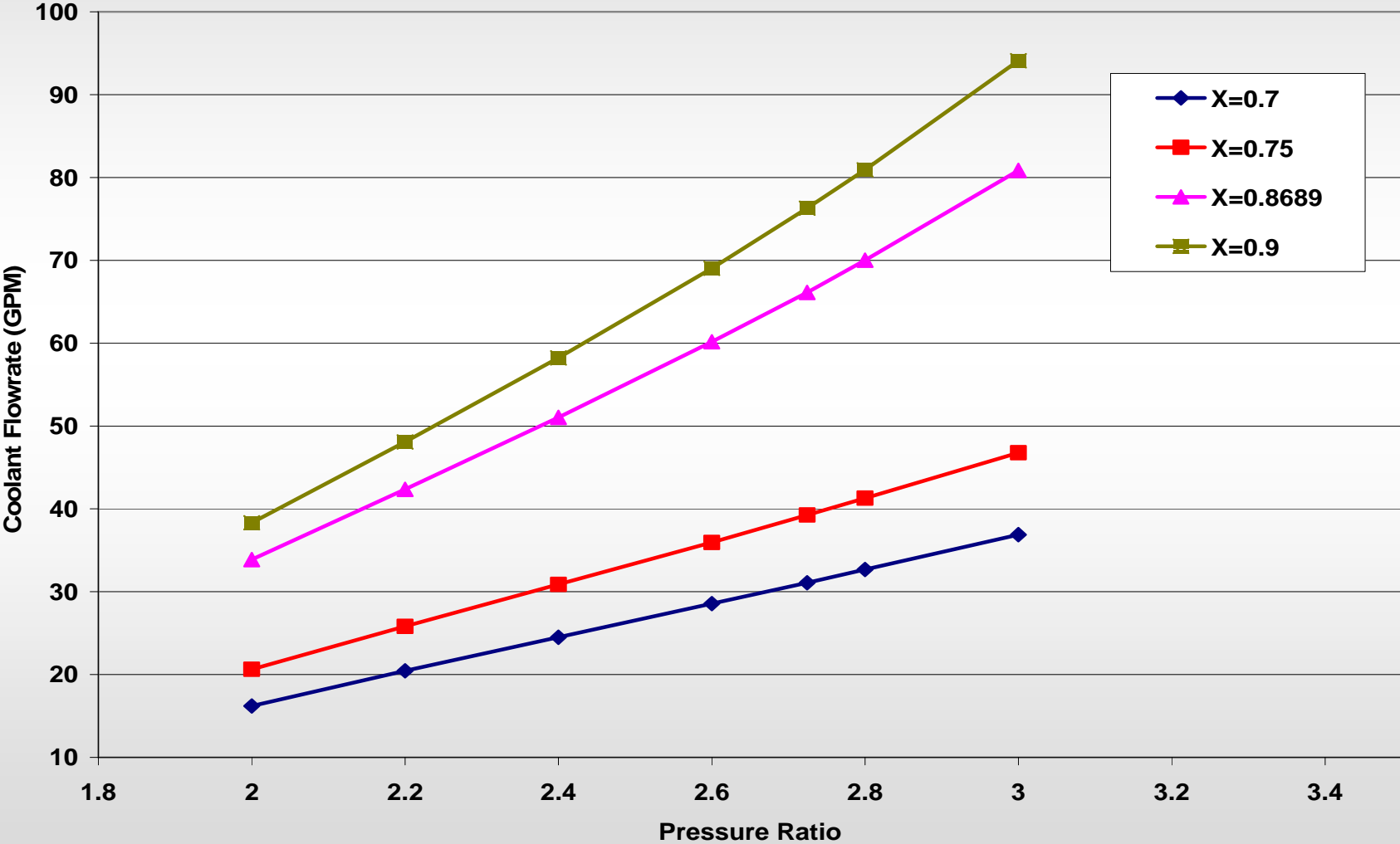
Heat Source: Efficiency versus Source Flow Rate and Ammonia Concentration



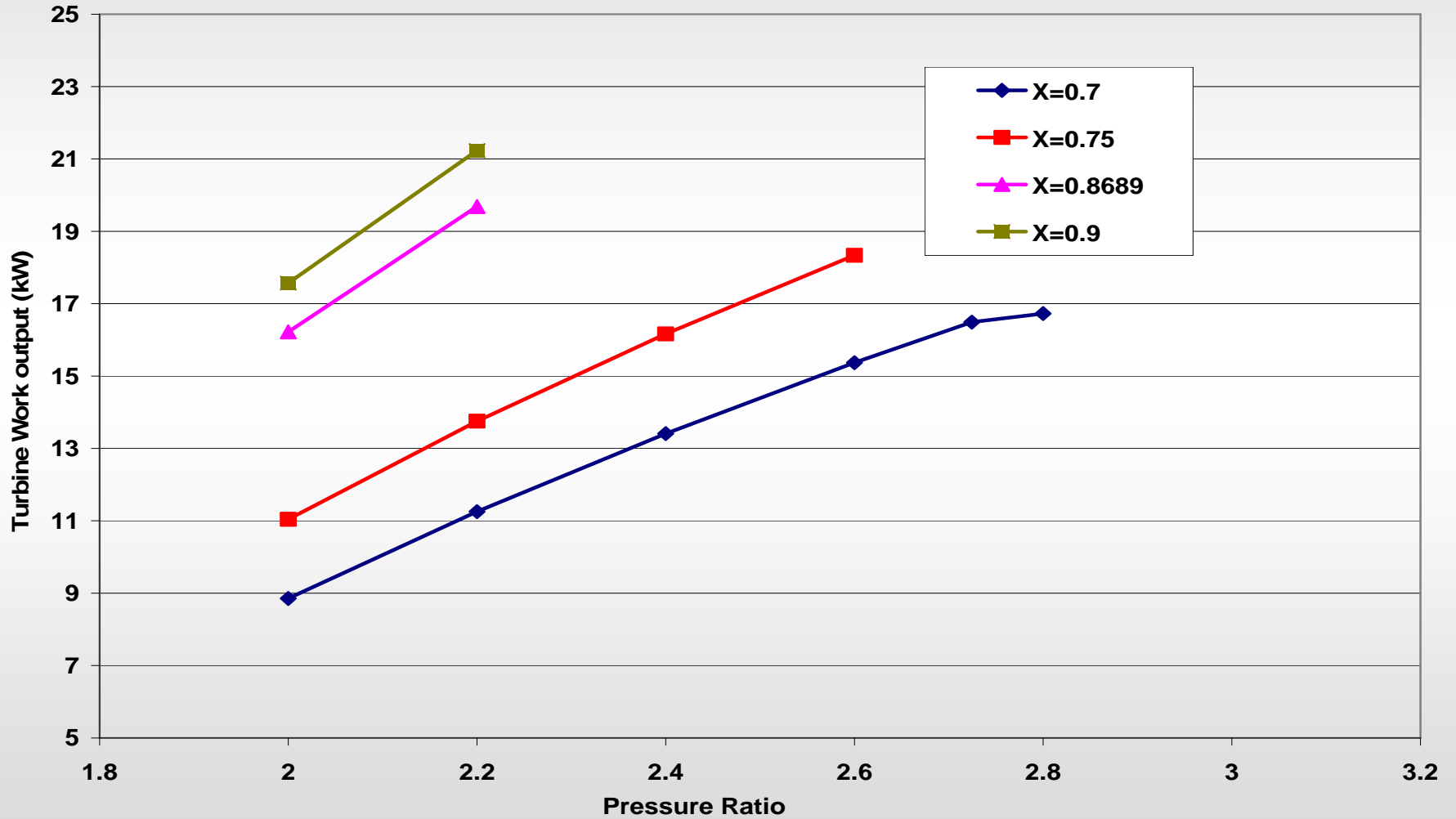
Heat Sink: Turbine work vs. Pressure ratio for and Ammonia Concentration for cooling temperature of 40°F



Heat Sink: Coolant flow rate vs. Pressure ratio and Ammonia Concentration for Cooling temperature of 40°F



Heat Sink: Turbine work vs. Pressure ratio and Ammonia Concentration for cooling temperature of 100°F



System Map

Major Components:

Heat source, heat sink, power system.
Assumptions and calibration.

Selected Independent Parameters for Maps:

Heating fluid temperature and flow rate
Cooling fluid temperature
System ammonia concentration and turbine
pressure drop.

Dependent Parameters:

System net efficiency, turbine work, input heat rate,
cooling flow rate, cooling rate.
(More if needed)

Design Consideration and Testing (Operation) Components Selection

Heat exchanger size

Ammonia concentration

Fluid flow controls

Pumps

Cooling device for heat sink

(e.g. dry cooler, cooling tower, river, ground water)

Heat source temperature

Screw expander characteristics

ORC System - Soon

Performance

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Electrical Output kWe (kW _e)	Water Heat Conditions				Condensing Conditions	
	Inlet Temp °C	Outlet Temp °C	Flow Rate GPM	Flow Rate m ³ /hour	Inlet Temp °C	Condensing Load kW
70	200	173	1-275-000	1-20	70	1-775-000
300	200	173	1-275-000	1-270	70	1-800-000

This system is designed to be used in conjunction with a low temperature heat source.

Electrical Output kWe (kW _e)	Water Heat Conditions			Condensing Conditions	
	Inlet Temp °C	Outlet Temp °C	Flow Rate m ³ /hour	Inlet Temp °C	Condensing Load kW
70	73	73.2	270	20	220
300	73	73.2	3-710	3.37	3-237

This system is designed to be used in conjunction with a low temperature heat source.

Electrical Output kWe (kW _e)	Water Heat Conditions					
	Inlet Temp °C	Outlet Temp °C	Flow Rate m ³ /hour	Inlet Temp °C	Outlet Temp °C	Condensing Load kW
70	20-200	10-200	0-800	3-100	3-100	2-700
300	20-200	10-200	0-800	21-800	21-800	23-130

This system is designed to be used in conjunction with a low temperature heat source. Water Heat Conditions are based on a 100°C inlet and a 100°C outlet. Condensing Conditions are based on a 100°C inlet and a 100°C outlet.

Electrical Output kWe (kW _e)	Water Heat Conditions						
	Inlet Temp °C	Outlet Temp °C	Flow Rate m ³ /hour	Inlet Temp °C	Outlet Temp °C	Flow Rate m ³ /hour	Condensing Load kW
70	30-300	15-300	1-2-800	3-800	7-700	0-700	3-300
300	30-300	15-300	1-2-800	20-100	20-700	0-100	3-300

This system is designed to be used in conjunction with a low temperature heat source. Water Heat Conditions are based on a 100°C inlet and a 100°C outlet. Condensing Conditions are based on a 100°C inlet and a 100°C outlet.

Electrical Output kWe (kW _e)	Saturated Steam Flow Requirements			
	Bar/Inch at and to 212°F @ 14.69 psia		kg/Inch at and to 100°C @ 101.31 kPa	
70	30	300	70	300
300	3-138	21-380	778	3-380

Electrical Output kWe (kW _e)	Pressure to Power			
	Inlet Pressure	Outlet Pressure	Flow (kg/s)	Flow (m ³ /hour)
100 kW	2100psi/14.3bar	870psi/6.0bar	11.8	11.7
2300 kW	8000psi/55.5bar	1000psi/7.0bar	28	28.807

This system is designed to be used in conjunction with a low temperature heat source.



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